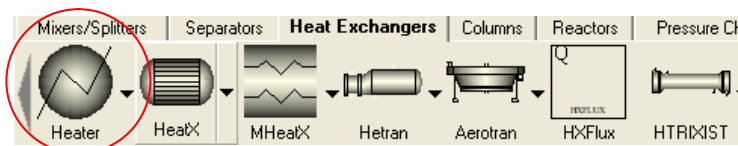
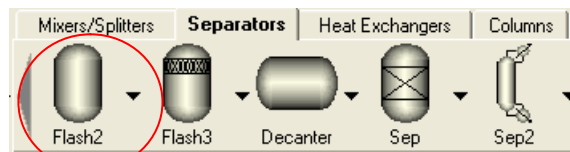
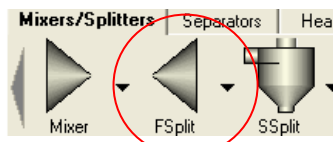
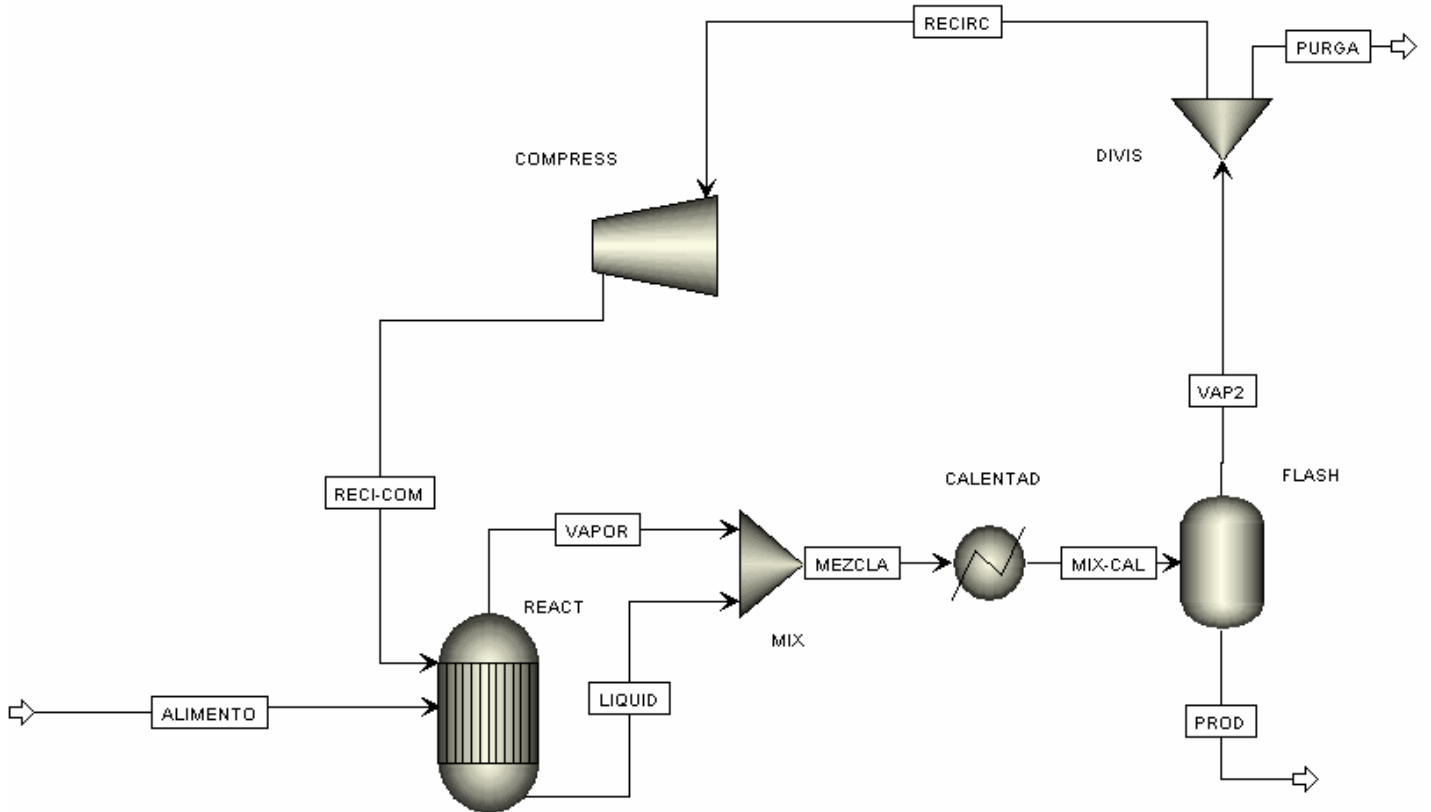


REACTOR DE AMONIACO CON RECICLO

Obtenga el siguiente diagrama de flujo:



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Seleccione los componentes:

Component ID	Type	Component name	Formula
N2	Conventional	NITROGEN	N2
H2	Conventional	HYDROGEN	H2
NH3	Conventional	AMMONIA	H3N
AR	Conventional	ARGON	AR
CH4	Conventional	METHANE	CH4
*			

Seleccione el método base CHAO SEADER:

Property methods & models

Process type: ALL

Base method: CHAO-SEA

Henry components:

Petroleum calculation options

Free-water method: STEAM-TA

Water solubility: 3

Electrolyte calculation options

Chemistry ID:

Use true-components

Property method: CHAO-SEA

Modify property models

Vapor EOS: ESRK

Data set: 1

Liquid gamma: GMXSH

Data set: 1

Liquid enthalpy: HLMX13

Liquid volume: VLMX20

Poynting correction

Heat of mixing

oprima y complete la información del ALIMENTO:

Substream name: MIXED

Ref Temperature

State variables

Temperature: 77 F

Pressure: 200 atm

Total flow: Mole lbmol/hr

Composition

Mole-Flow lbmol/hr

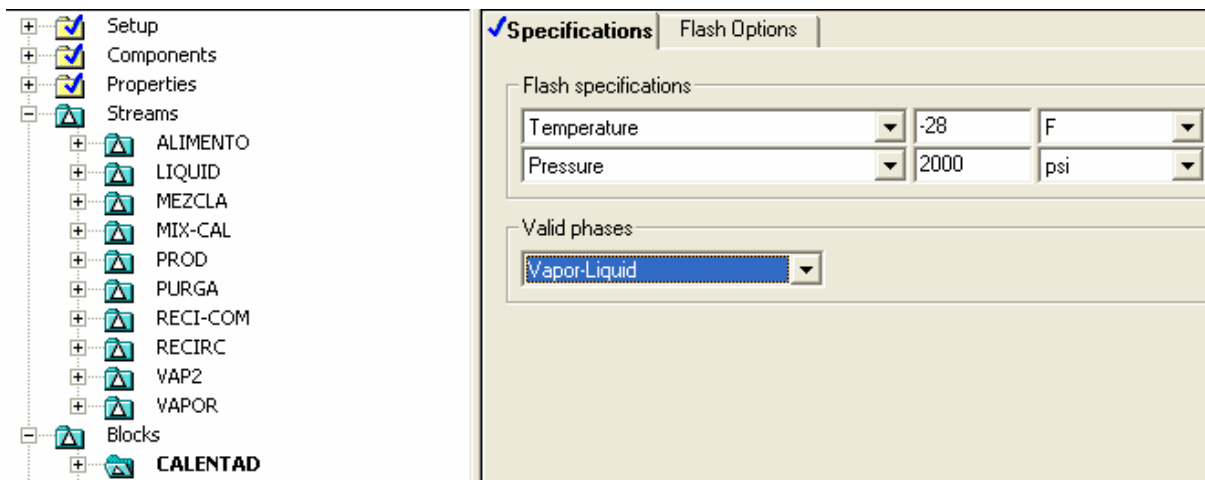
Component	Value
N2	24
H2	74,3
NH3	0
AR	0,6
CH4	1,1


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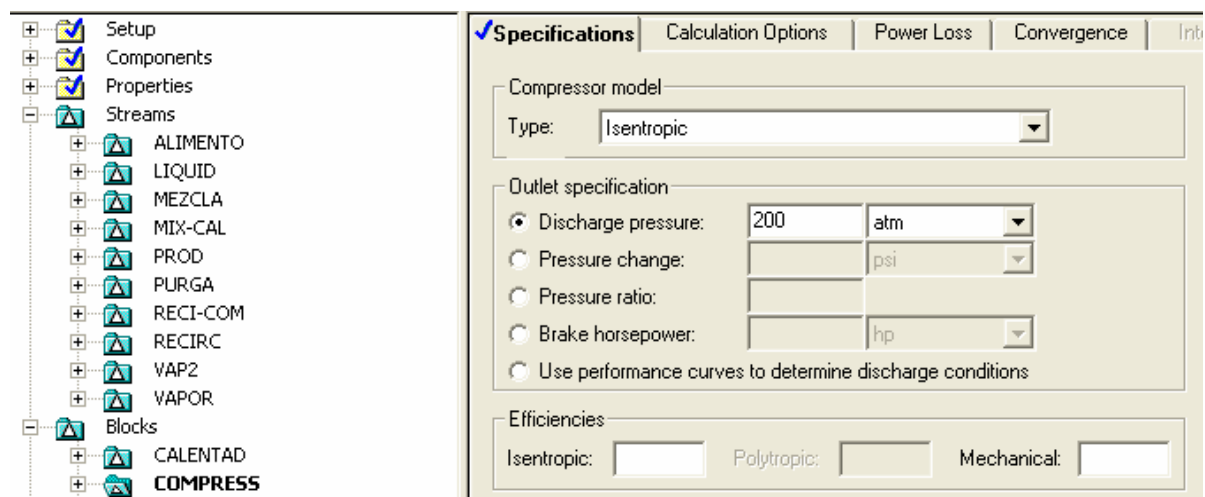
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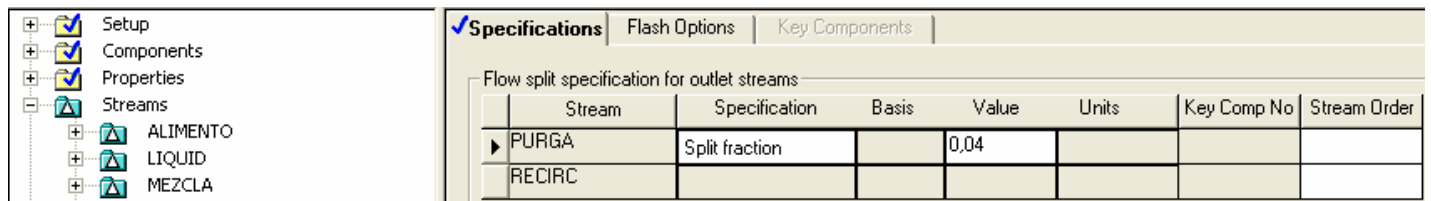
oprima  y complete la información del bloque CALENTAD:



oprima  y complete la información del bloque COMPRESS:



oprima  y complete la información del bloque DIVIS:



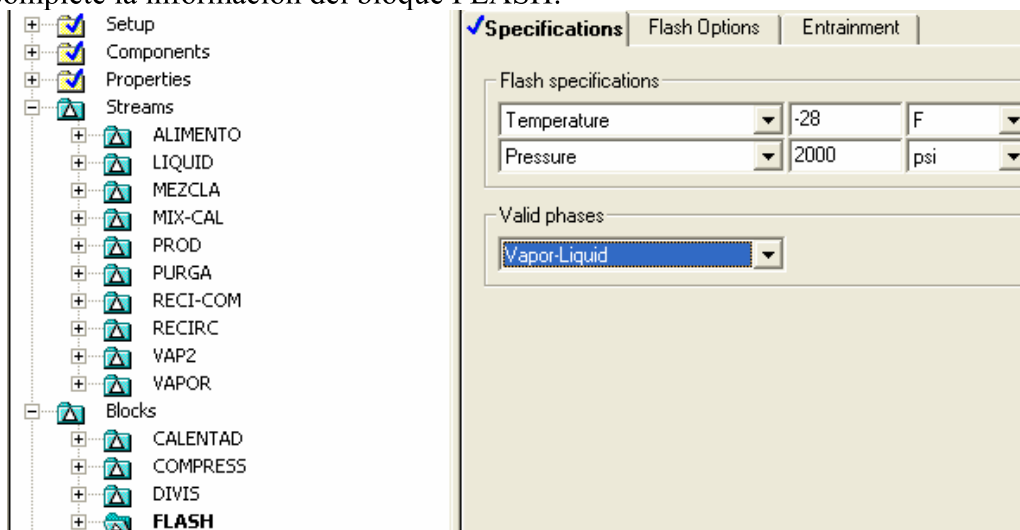
Stream	Specification	Basis	Value	Units	Key Comp No	Stream Order
PURGA	Split fraction		0,04			
RECIRC						


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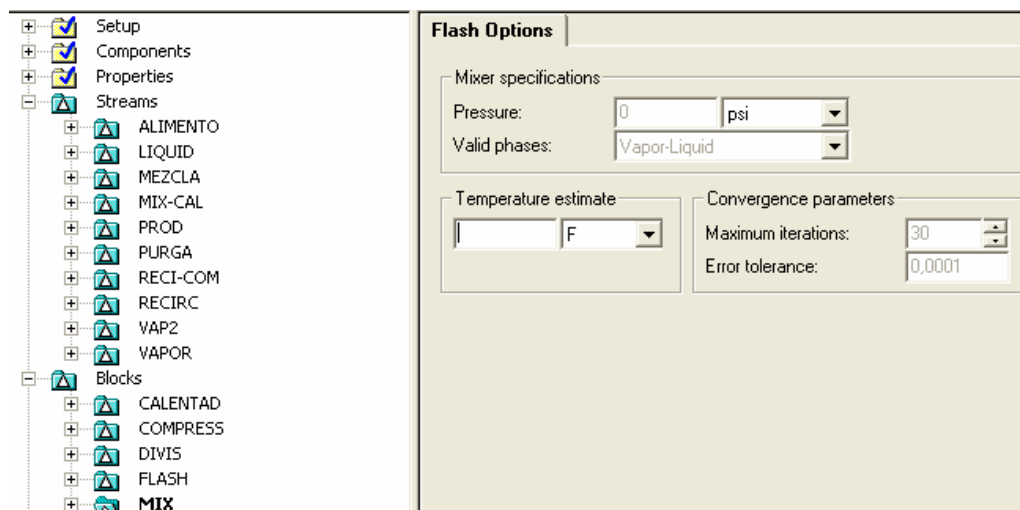
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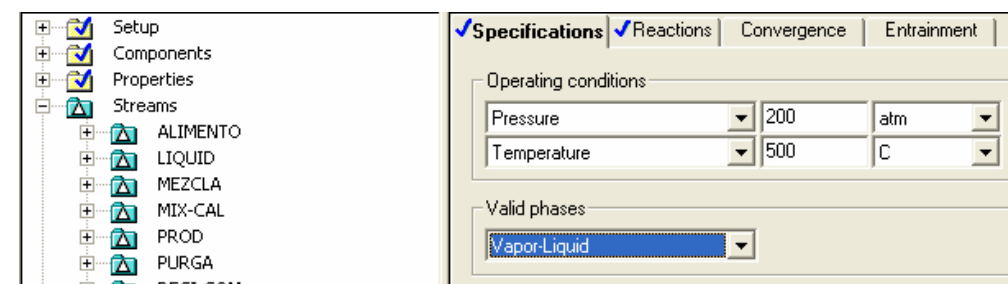
oprima  y complete la información del bloque FLASH:



oprima  y complete la información del bloque MIX:



oprima  y complete la información del bloque REACT:



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Cree un objeto REACTIONS y introduzca la reaccion:

Reaction No.: 1

Reactants		
Component	Coefficient	Solid
N2	-1	No
H2	-3	No
*		

Products		
Component	Coefficient	Solid
NH3	2	No
*		

Products generation:

Molar extent: [] lbmol/hr

Temperature approach: 0 F

Extent estimate: [] lbmol/hr

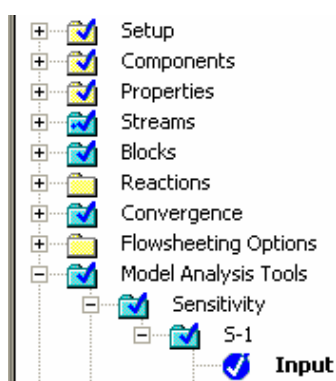
Buttons: [N>] [Close]

Determine products by specifying temperature approach to equilibrium.

El formulario debe aparecer así:

Rxn No.	Specification type	Stoichiometry
1	Temp. approach	N2 + 3 H2 <-> 2 NH3

Cree un objeto sensitivity y cambie la relacion de flujos en el divisor:



Flowsheet variable	Definition
FAMONI	Mole-Flow Stream=PROD Substream=MIXED Component=NH3
XARG	Mole-Frac Stream=PURGA Substream=MIXED Component=AR
PURGA	Stream-Var Stream=PURGA Substream=MIXED Variable=MOLE-FLOW
RECICL	Stream-Var Stream=RECIRC Substream=MIXED Variable=MOLE-FLOW
XMETAN	Mass-Frac Stream=PURGA Substream=MIXED Component=CH4
*	

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Define Vary Tabulate Fortran Declarations Optional

Variable number: 1

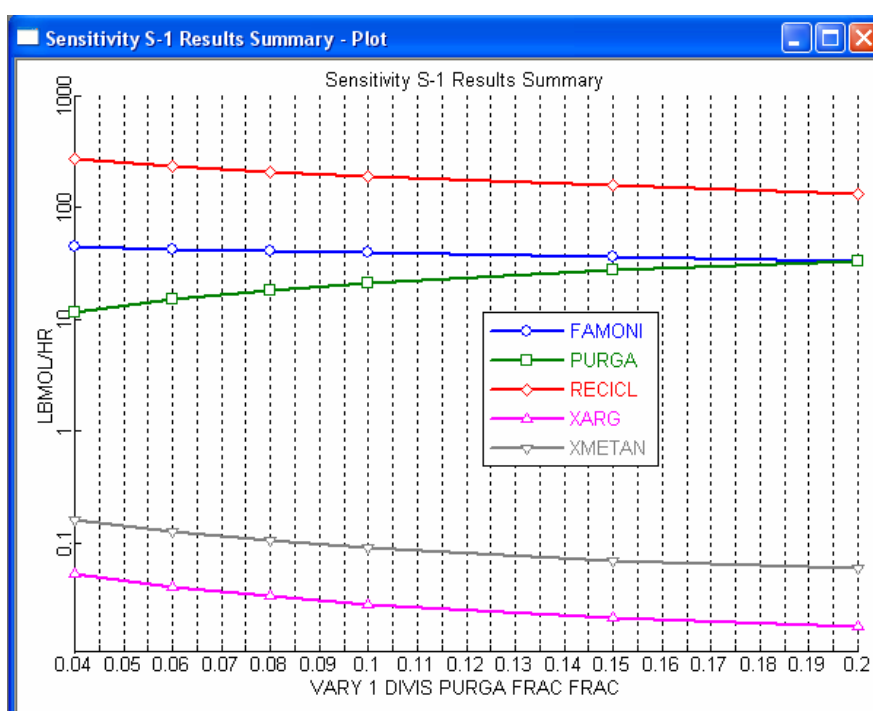
Manipulated variable
 Type: Block-Var
 Block: DIVIS
 Variable: FLOW/FRA
 Sentence: FLOW/FRA
 ID1: PURGA

Values for varied variable
 List of values

0,2	0,15	0,1	0,08	0,06	0,04
-----	------	-----	------	------	------

 Overall range
 Lower:
 Upper:
 #Point: Incr:

Report labels
 Line 1: Line 2:
 Line 3: Line 4:



Las composiciones de Argon y Metano aumentan al disminuir la purga y ellas son muy grandes respecto a las del alimento, esto es, si la relación purga/reciclo disminuye, el efluente vapor del flash llega a ser mas rico en los componentes inertes, sin embargo esto incrementa el flujo del reciclado y el costo de recirculación (además del volumen del reactor).

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